THERMODYNAMIC PARAMETERS AND STABILITIES OF SOME RARE-EARTH METAL ION CHELATES OF α -VALINE

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Solution equilibria for some rare-earth metal ions with value have been studied potentiometrically in aqueous medium at temperatures from 25 to 55° and ionic strengths (I) from 0.1 to 1.0 mol dm⁻³ NaClO₄. The thermodynamic parameters ΔH^{\pm} , ΔS^{\pm} and ΔG^{\pm} for the formation processes were evaluated in terms of temperature, ionic strength and nature of metal ion present. The stability of the complexes was found to be : La(III) < Nd(III) < Gd(III) < Eu(III) < Yb(III) < Lu (III).

Key words: Formation constant, Thermodynamic parameters, Rare-earths.

Introduction

Amino acids play a significant role in biochemistry and chemical industry as starting material for manufacturing, proteins, peptide, coenzyme, drugs and antibiotics [5-10]. However, there have only been a few studies on their complexes with rare earth metal ions [11-13]. In the present work the interaction of α -valine as with the example of α -amino carboxylic acids rare-earths La(III), Nd(III), Eu(III), Gd(III), Yb(III) and Lu(III) in aqueous medium have been studied potentiometrically at different temperatures and ionic strengths. The stability constants of the complexes were evaluated employing different methods [14,15, 19]. As well as the corresponding thermodynamie parameters ΔH^{\pm} , ΔS^{\pm} and ΔG^{\pm} for the formation processes have been calculated and discussed in order to give information about the nature of the complexes.

Experimental

All chemical used in this work were of BDH or Analar grade. The metal content in the solutions was determined as recommended [16], solutions of lower concentration were obtained by dilutions. The measurement of pH values were carried out using pH meter (HANNA instrument, Italy) with accuracy of 0.02 log unit and sensitivity \pm 0.01, temperature was controlled by a thermostated water-bath (\pm 0.1°).

The proton-ligand and metal-ligand thermodynamic stability constant were calculated from the results of the following solutions against standardised carbonate-free KOH solution (0.159 mol dm⁻³).

(i). $HClO_4$ (0.02 mol dm⁻³) + NaClO₄ (2 mol dm⁻³)

(ii). Solution (i) + valine $(0.02 \text{ mol dm}^{-3})$

(iii). Solution (ii) + metal solution $(0.004 \text{ mol dm}^{-3})$

The total volume was made to 50 cm³ in each case with doubly distilled water and the titrations were carried out in a specially designed double-walled beaker (250 cm³, Pyrex) using the Calvin-Bejerrum [17] titration technique as modified by Irving and Rossotti [14,15] and performed in duplicate in order to establish reproducibility.

Results and Discussion

In order to examine the influence of temperature and ionic strength of the medium on the dissociation process of α -value, the potentiometric curves of α -value solutions at temp. from 25 to 55° and ionic strengths from 0.1 to 1.0 mol dm⁻³ NaClO₄ were determined (Fig. 1). The value obtained were in good agreement with those reported in the literature [9,11]. From these curves and by the application of Bejrrum's method and its modifications [14,15,17] the values of pK were calculated (Table 1). The values obtained were in good agreement with those reported in the literature [9,11]. The results, indicate that pK values increases with the increase in ionic strength. On the other hand, pK, values decrease with a rise in temperature in accordance with the weak acidic nature of valine. Decreasing pK, values with rise in temperature support the hypothesis that, the dissociation process is favourable at higher temperature.

Plotting log K_a vs the square root values of ionic strength (I^{1/2}), a straight line was obtained, its extrapolation at 1 = 0, log k_o value was evaluated. The free energy ΔG^{\pm} values of the dissociation process can be obtained from the relation:

$\Delta G^{\neq} = -2.303 \text{ RT log k}_{o}$

The ΔG^{\pm} values were positive; therefore, the dissociation process is non-spontaneous. ΔG^{\pm} values increases with increase in temperatures (Table 1). A straight line was obtained of plots of log k_o -1/T for each ionic strength. The slope and intercept of the line gap the correspondence ΔH^{\pm} and ΔS^{\pm} for the dissociation process respectively (Table 1). The enthalpy changes ΔH^{\pm} were positive values as expected for the weak acid nature of α -valine and the dissociation process is an endothermic reaction. On the other hand, entropy change values ΔS^{\star} were negative; this means that the dissociation process was accompanied by the decrease in the disorder of the system. This observation may be due to the solvation effect and Zweiter ion formation [19].

The interaction of rare-earths (M³⁺) with α -valine (H₂L) may be represented as:

$$M^{3+} + H_2 L \xleftarrow{k_1} ML^+ + 2H^+$$
$$ML^+ + H_2 L \xleftarrow{k_2} ML^-_2 + 2H^+$$

To investigates the effect of the working condition on the pK_a , value series of pH-metric titration of α -valine (H₂L)-in aqueous medium at different temperature from 25 to 55° and varying ionic strength 0.1-1.0 mol dm³ NaClO₄ were carried out as an example (Fig. 1). The average number of proton associated with α -valine was calculated according to the following equation.

$$\overline{n}_{A} = Y + \frac{(V_{1} - V_{2}) N^{\circ} + E^{\circ}}{(V_{o} + V_{1}) T_{L}}$$

The average number of α -valine per metal ion, PL, were calculated using the following equations

$$\overline{n} = \frac{(V_3 - V_2) N^\circ + E^\circ}{(V_o + V_1) \overline{n}_A \cdot T_M}$$
$$pL = \log \begin{bmatrix} \sum_{n=0}^{n=1} \beta_1 (\log [H^+]^n] \\ T_L - \overline{n} T_M \end{bmatrix} \frac{V_o + V_3}{V_o}$$

The parameters \overline{n} , n_A and pL having the same definations and meanings given by Irving-Rossotti [14,15], where T_L , T_M

Table 1. Influence of the Temperature and Ionic Strength of the Medium on PK_a Values of α -Value, as well as

Some Thermodynamic Parameters for its

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						No. 20	
Ionic strength	1	pK valu	ues (°C)		ΔH^{\pm}	-ΔS [≠]	
mol dm ⁻³	25°	350	45°	55°	(kJ mol ⁻¹)	(JK-1 mol-1)	
0.1	9.45	9.36	9.28	9.21	14.99	130.6	
0.2	9.47	9.39	9.31	9.24	14.35	133.17	
0.4	9.51	9.44	9.36	9.29	13.72	136.04	
0.8	9.56	9.50	9.42	9.35	13.10	137.04	
1.0	9.58	9.53	9.45	9.38	12.48	141.00	
pK	9.37	9.28	9.20	9.14	1.5 - 5.6 -	44 - 14 - 10	
∆G≠	53.46	54.73	56.01	57.39	a manathin		
(kJ mol ⁻¹)				(10) i			

and β are the total concentration of ligand, metal and the overall stability constant of complexes respectively. The values of n for all complexes varying between 0.2 – 1.9 thereby indicating the formation of 1:1 and 1:2 (M:L) complexes.

Plot (\bar{n} -PL) diagrams for the complexes at different ionic strengths gap the formation curves represented in Fig. 2. From these curves log k_1 and log k_2 can be evaluated at n equal to 0.5 and 1.5 respectively. Values of the overall stability constant $\beta(\beta=k_1k_2)$ of the complexes were further refined by using calculation method graphical, least-square and the mid-point methods calculation methods. The final values of the overall stability constant (log β) for the complexes are given in (Table 2). The results are in good agreement with those from similar studies [11-13].

The results indicate that the stability constant decreases with the increases in temperature and thus lower temperatures favour complex formation. On the other hand (log β) values decrease with the increases in the ionic strength. This observation may be due to the decrease in the metal ion activity for the complexation with the ligand in the presence of other foreign ions in the system i.e. the metal ions are screened by the other



Fig. 1. Potentiometric titration curves at $\mu = 0.1M$ for α -valine with metal ions

ions, this conclusion is in accordance with similar findings reported by Hückel [20].

The values of the overall stability constant for the complexes increased in the order: $La(III) < Nd(III) < Gd(III) \le$ Eu(III) < Yb(III) < Lu(III), which is in accordance with the Irving-Williams rule [21]. A plausible explanation for this trend is that, rare-earth metal ions differ in the number of 4F electorns which are effectively shielded from the interaction with the ligand orbitals by the electrons in 5s and 6p orbitals. Figure 3 shows that the difference in stability constants of rare earth metal ion complexes and the positive nuclear charge of metal ions e.g. Gd(III) ion has completely half filled thus configuration leads to a shielding of the nuclear charges of such ion from the interaction with the ligand and hence to decrease its (log β) than that of Eu(III) the next metal ion in series. The trend of stability is in accordance with the increase of the effective ionic potential (Z²/r) of the metal ion in the same direction [22].



(a) La (III); (b) Nd (III), (c) Eu (III), (d) Gd (III), (e) Yb (III), (f) Lu (III).



Fig. 3. Log β as a function of ionic potential ($\mathbb{Z}^2/_1$) for value-lanthanide complexes at I = 1 moldm³ NaClO₄ and different temperatures.



Fig. 4. Relation of log β -1/T for α -valine complexes at different ionic strengths.



$\Delta G^* = -2.303 \text{ RT} \log \beta_o$

All obtained values were negative (Table 3) which indicated the spontaneous reaction nature of valine with lanthanide ions and ΔG^* increases from La(III) to Lu(III) which indicated that the stability of the complexes increase in the same order.

Plotting, $\log \beta$ vs 1/T gave a straight line (Fig. 4) its slope and ordinate yield ΔH^{*} and ΔS^{*} for the complexation process respectively, according to the reaction:



Metal ion (III)						
I(mol dm ⁻³)	La	Nd bolon	nom Eu	Gd	Yb	Lu
t(°C)	ion to obtain the	e following equal	di ni bônu	115 3 22		11
25°C						
0.1	9.82	10.21	10.57	10.52	11.43	11.50
0.2	9.79	10.17	10.53	10.48	11.39	11.46
0.4	9.71	10.08	10.43	10.36	11.29	11.36
0.8	9.65	10.02	10.36	10.30	11.22	11.29
1.0	9.61	9.97	10.31	10.25	11.17	11.24
35°C						
0.1	975	10.13	10.48	10 44	11.35	11.43
0.2	9.72	10.09	10.44	10.39	11.31	11.38
0.4	9.63	9.99	10.35	10.29	11.21	11.28
0.8	9.56	9.93	10.27	10.20	11.33	11.19
1.0	9.52	9.89	10.23	10.15	11.08	11.15
150						
0.1	9.68	10.05	10.41	10.38	11.27	11.36
0.2	9.65	9.99	10.36	10.33	11.22	11.30
0.4	9.55	9.91	10.27	10.21	11.12	11.20
0.8	9.48	9.85	10.19	10.14	11.05	11.11
1.0	9.44	9.81	10.15	10.08	11.00	11.07
50						
01	9.61	9.96	10.34	10.29	11.18	11 28
0.2	9.58	9.91	10.28	10.22	11.10	11.20
0.4	9.48	9.82	10.20	10.13	11.04	11.23
0.8	9 40	9 77	10.02	10.07	10.97	11.03
1.0	9 36	9 73	10.02	10.02	10.92	10.99

TABLE 2. THE OVERALL STABILITY CONSTANTS (log β) of 1:2 M³⁺ Value Complexes at Different Ionic Strengths and Temperature

		log	K	57.41 Tr.	100	-∆G* (I	kJ mol ⁻¹⁾	
Metal t(°C) ion	25	35	45	55	25	35	45	55
La (III)	9.92	9.86	9.79	9.72	56.58	58.13	59.62	61.10
Nd (III)	10.32	10.24	10.16	10.07	58.90	60.40	61.87	63.22
Eu (III)	10.69	10.60	10.53	10.46	61.00	62.49	64.12	65.70
Gd (III)	10.64	10.57	10.52	10.41	60.74	62.36	64.05	65.41
Yb (III)	11.55	11.47	11.39	11.30	65.90	67.67	69.38	70.97
Lu (III)	11.62	11.56	11.49	11.41	66.30	68.17	69.98	71.68

TABLE 4. ENTHALPY AND ENTROPY CHANGE OF METAL ION-VALINE COMPLEXES AT DIFFERENT IONIC STRENGTHS.

	-ΔH≠ (kJ mol ⁻¹)				10.0	-ΔS≠ (kJ mol ⁻¹⁾				
I (mol dm ⁻³) Metal ion	0.1	0.2	0.4	0.8	1.0	0.1 (M) (D ra	0.2	0.4	0.8	1.0
La (III)	13.10	12.79	14.35	15.60	15.28	144.06	143.48	137.77	132.40	132.62
Nd (III)	15.60	16.22	15.91	15.28	14.97	143.16	140.30	139.52	140.46	140.65
Eu (III)	14.35	15.60	15.28	14.97	14.93	154.23	149.28	148.30	148.12	149.26
Gd (III)	15.35	14.97	14.04	14.35	14.66	153.28	150.42	151.16	149.07	147.07
Yb (III)	15.59	15.28	14.97	15.28	15.31	166.51	166.70	165.74	164.40	162.48
Lu (III)	13.72	14.34	14.97	16.22	15.60	174.14	171.27	167.27	161.67	162.88

$$\log \beta = \frac{-\Delta H^{*}}{2.303 \text{ R}} = \frac{1}{T} + \frac{\Delta S^{*}}{2.303 \text{ R}}$$

The ΔH^* and ΔS^* values for all complexes are summarized in Table 4. From Table 4, it is clear that the values of ΔH^* for all cases are negative which means that the complexation processes are exothermic reactions and are favourable at lower temperatures. On the other hand, ΔS^* values for all complexes are positive, which suggests that, on account of the complexation processes the disorder of the system increases and the entropy factor is the principle driving force for the complex.

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670 (1977).

The aim of the present work is to achieve the above described objective. For this purpose, two models have been proposed as follows:-

Fast regimes model. Since the reactions in the pseudo 1st order fast, instantaneous and intermediate regimes occur very rapidly in the film, the gascous component is never present in the bulk of the liquid. These regimes are generally classified together as fast regimes and have been incorporated into a single model which has then been used to minimise the gas consumption. In mathematical terms the equation relating the concentrations of B in the bulk of the liquid with time is given by:

$$\frac{dC_B}{di} = N_{BL} \left(u_0 / \varphi \right) - (b' / a') K C_A C_B \qquad (1)$$

With initial conditions $t = O, C_a = O, C_b = C_{to}$ in all regimes the molar flux of B from the balk into the

film is then determined by :-

 $N_{R} = -(b'/a) (N_{R} - N_{R})$

. $N_{\rm AL} = 0$ in all cases, where

 $N_{ij} = K_{off} P_{ab}$ (for fast pseudo 1st order reaction)...(3) Where K_{ab} is a modified overall mass transfer coefficient

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intermodulte and instantaneous reactions. I hear reguees are described by concentration gradients shown in Figs. 1-5 Optimization studies were made on this model and it was found that the slow regimes gave significant savings in gas consumption when operating with an optimal gas rate policy compared with using a best constant gas rate.

Experimental

Optimization. Optimisation pervades the field of science, origineering and business. A process can be represented by some equations or perhaps solely by experimental data. There is also a single performance criterion or objective function in mind such as minimum cost. The goal of optimisation is to find the values of the variables in the process that yield the best value of the performance criterion. The ingrediants described above - process or model and the performance criterion comprise the optimisation "problem".

Optimization of gas-liquid remt-batch stirned tank reactor. Optimization problems can unise in both the design and operation of the reaction [1]. The most significant variables affecting the type of reactor considered here are gas flow rate, stirner speed, temporature and pressure. Since the present system has been assumed to be isothermal and isobaric and stirrer speed has also been assumed to be unchanged during the