# PAKISTAN JOURNAL <br> OF <br> SCIENTIFIC AND INDUSTRIAL RESEARCH 

Vol. 9, No. 3 July 1966

# TEMPERATURE DERIVATIVES OF VISCOSITY, DENSITY AND REFRACTIVE INDEX FOR THE WATER-ETHANOL SYSTEM 

# Part II.-Further Measurements on the Activation Energy of Viscous Flow for Aqueous Ethanol in the Concentration Range of o to $\mathbf{5} \%$ 

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(Received February 19, 1966)


#### Abstract

A detailed examination of the concentration dependence of the jumps in $\mathrm{E}_{\boldsymbol{i}}$ for several aqueous solutions from $0 \%$ to $5 \%$ ethanol is undertaken at increments of nearly $0.9 \%$ ethanol. En is obtained by using the Andrade equation after differentiation, viz. $$
\mathrm{En}_{n} ; \mathrm{R}=\Delta \ln \eta / \Delta\left(\frac{1}{\stackrel{1}{T}}\right)=-\mathrm{T}^{2} \Delta \ln v_{i} / \Delta \mathrm{T}
$$


For studying the course of the movements of these energy jumps as a function of alcohol concentration, a chart is prepared for the various energy jumps, which are classified as large, medium or small compared to mean value of $(\Delta E / R) /$ $1000=0.07$. The shifts of these jumps with the concentration changes are mostly smooth, in agreement with the ideas advanced earlier, but there is evidence for branching of these discontinuities into pairs at certain alcohol concentrations. This is accompanied by appearance and disappearance of certain jumps, so that in these regions the detailed chart looks substantially different from the earlier one based on data at interval of about $2 \%$ ethanol.

## Introduction

The existence of sharp jumps in the activation energy of viscous flow En has been established on a firm footing in the case of several liquids, such as water, ${ }^{1}$ ethylene glycol, ${ }^{2}$ light hydrocarbons ${ }^{3}$ and mineral oils. 4 Similar jumps were found in a series of experiments on dilute aqueous ethanol 5 and it was confirmed that En remains sensibly constant over certain temperature ranges and then sharply drops from one stage to the next. It was noted, that in the concentration range from $2.5 \%$ to $30 \%$ alcohol, these jumps occur at intervals of $4^{\circ} \mathrm{C}$. to $8^{\circ} \mathrm{C}$., and the magnitude of $\Delta \mathrm{E}$ at each jump is of the order of 0.1 to $0.3 \mathrm{cal} . /$ mole. To further investigate the character of these jumps, the concentration range from $0 \%$ to $11 \%$ has been examined by Ahsanullah and Qurashi ${ }^{6}$ (1965) by working with three more solutions of intermediate concentrations, namely $2.5 \%, 6.9 \%$ and $9.2 \%$, so as to trace out the course of these jumps as a function of concentration. It appeared possible that these movements of the jumps might be discontinuous in character, especially in the region of $26^{\circ} \mathrm{C}$. to $42^{\circ} \mathrm{C}$. and for $2.5 \%$ to $6 \%$ ethanol solutions.

Lately, the derivatives of refractive index $\mathrm{dn} / \mathrm{dt}$, and of coefficient of dilatation, in addition to that
of viscosity, have been the subject of investigation in this laboratory, and it was observed in Part I of the present series of papers that the temperatures at the minimum of ( $-\mathrm{dn} / \mathrm{dt}$ ) values for five solutions of ethanol in water were quite close to the sharp jumps in En of that particular concentration, thus establishing a degree of correspondence between these two phenomena. Tentative charts, each containing series of graphs (Fig. I) showing the variation of temperature for a particular energy jump (and minimum observed in -dn/dt) were prepared for $3 \%$ to $11 \%$ ethanol. This generally confirmed the earlier results, but the concentration intervals used were fairly large, viz., of the order of $2 \%$ ethanol, thus leaving room for ambiguity in several regions. In order to further elucidate these phenomena and the nature of these transitions or discontinuities, it was considered worthwhile to undertake a detailed study of the jumps of En in the concentration range of o to $5 \%$ ethanol. The present communication describes some accurate measurements with dilute aqueous ethanol solutions covering the whole range of o to $5 \%$ in six increments of nearly $0.9 \%$ alcohol each. New activation energy measurements have been made on $0.9 \%, 1.8 \%, 3.5 \%$ and $4.1 \%$ ethanol solutions, each set being performed with a temperature interval of $I^{\circ} \mathrm{C}$. between successive observations.


Fig. 1.-Reproduction of the plot of jumps in $E$ and minima in (-dn/dt) from the earlier work of Qureshi, Haider and Qurashi, for some ethanol solutions from $2 \%$ to $11 \%$. (a) Temperature-concentration charts, showing the dependence of a particular minimum of (-dn/dt) and corresponding energy jumps on the concentration of the alcohol. The hollow circles are for the temperaturc obtained from the jumps in $\mathrm{E} / \mathrm{R}$ and the crosses are for the temperature for the minima of ( $-\mathrm{dn} / \mathrm{dt}$ ). (b) Corresponding charts for the maxima of ( $-\mathrm{dn} / \mathrm{dt}$ ) and middle points of the regions of constant energy. The crosses are for the maxima of ( $-\mathrm{dn} / \mathrm{dt}$ ) and solid circles are for the mean of the values from $\mathrm{dn} / \mathrm{dt}$ and $E / R$ graphs. The graphs of Figs. 1 (a) and (b) show anomalies in region of $26^{\circ} \mathrm{C}$. to $42^{\circ} \mathrm{C}$. and for the portion near $3.5 \%$ ethanol solution.

## Experimental Technique

The experimental procedure is essentially the same as adopted before for the En measurements on water and glycol, and discussed in detail for dilute alcohol by Ahsanullah and Qurashi. ${ }^{6}$ Contrary to the usual practice of measuring the slope of the tangent at various points in question on the plot of $\ln n$ against $1 / T$, the value of $\mathrm{E}_{\mathrm{n}}$ is determined by measuring the kinematic viscosity with high precision at close temperature intervals; this interval is nearly $I^{\circ} \mathrm{C}$. in the present case. (This differential technique has the advantage of eliminating the uncertainty in drawing tangents as well as the error in the calibration of stop watches and adjustment of liquid level after every reading). The activation energy $\mathrm{E} \eta$ is obtained from the differential of Andrade equation:

$$
\begin{gathered}
\eta=\mathrm{A} \exp \mathrm{En} / \mathrm{RT} \\
i . e \mathrm{E} \eta / \mathrm{R}=\Delta \ln \eta / \Delta\left(\frac{\mathrm{I}}{\mathrm{~T}}\right)=-\mathrm{T}^{2} \Delta \ln \eta / \Delta \mathrm{T}=-\mathrm{T}^{2} \Delta \ln (\nu \times p) / \Delta \mathrm{T} \\
=-\mathrm{T}^{2} \Delta \ln \nu / \Delta \mathrm{T}+\mathrm{T}^{2} \beta=\frac{\mathrm{E} v}{\mathrm{R}}+\mathrm{T}^{2} \beta
\end{gathered}
$$

where $n$ is dynamic viscosity, $\rho$ is the density and $\beta$ is the coefficient of dilatation of the liquid. $\mathrm{T}^{2} \beta$ forms a small slowly-varying correction term.

The kinematic viscosities are obtained by measuring, with a calibrated stop watch reading to o. I second, the time of flow four to six times through a U-Tube Viscometer No. "I" (constant 0.0040I) of British Standard Specifications, supported vertically by a rigid clamp in a thermostat giving a temperature stability of $\pm 0.002^{\circ} \mathrm{C}$. or better. The actual temperature is read by ordinary mer*
cury thermometer graduated to one-tenth of a degree, while the interval $\Delta T$ is recorded over six degrees with a Beckmann differential thermometer, calibrated previously by intercalibration method. The height of the liquid meniscus at equilibrium above the fiducial mark on the large bulb of the viscometer is read by cathetometer to 0.001 cm . and appropriate correction is applied to flow time. Since the time of flow ranges from 200 to 600 seconds, and is read to $\pm 0.01$ second, all the above measures ensure a reproducibility of i in 40,000 or better, in the final value of viscosity.

The water content of each solution is checked and rechecked at various stages, especially at the beginning and at the end of each experiments by density and viscosity measurements, carried out at two to three different temperatures. When working at the higher temperatures, a ballast bottle, connected to the wide limb of the viscometer, was immersed inside the bath and held some of the particular solution used in the viscometer. ${ }^{\text {I }}$ This enables control of the evaporation of the test liquid by setting up a dynamic vapour equilibrium.

## Results on $0.9 \%$ and $\mathbf{r} . \mathbf{8} \%$ of Aqueous Ethanol

It was considered desirable to explore first the region between $0 \%$ and $2.5 \%$ ethanol content,
and for this purpose solutions containing $0.9 \%$ and $1.8 \%$ alcohol by weight were prepared by adding measured quantity of absolute ethanol to thrice-distilled conductivity water and were subjected to viscosity determination. Since the ethanol in these solutions is liable to evaporation to a significant extent at higher temperatures, resulting in significant change in the ethanol percentage, counter-measures were adopted by (i) using the ballast bottles mentioned earlier (ii) checking the alcohol content at different stages, so that overall deviation in the concentration during the whole course of experiments may not exceed $\pm 0.05 \%$ ethanol. The dilute solution containing $0.9 \%$ alcohol was subjected to flow activation energy measurements at the interval of $I^{\circ} \mathrm{C}$. in the temperature range of 10 to $60^{\circ} \mathrm{C}$., and Table $I(a)$ contains the values of $E / R \div 1000$ for rising and falling sequences deduced from the Beckmann readings, temperatures ${ }^{\circ} \mathrm{C}$. and time of flow (corrected for level). The $\mathrm{E} / \mathrm{R} \div$ iooo values are represented by the lower curve drawn through the solid circles of the Fig. 2, where the full line graph for pure water is shown shifted downward relative to the vertical scale by 0.2 unit of $E / R$ $\times$ 10-3 $^{3}$. There are a succession of the steps at nearly $4.5^{\circ} \mathrm{C}$. interval from $10^{\circ}$ to $60^{\circ} \mathrm{C}$. with árerage step depth of 0.09 unit of $E / R \div 1000$ while r.m.s. deviation is $\pm 0.004$ units.

Table I (a).—Measured Activation Energies E/R $\div 1000=-\left(T^{2} \Delta \ln \nu / \Delta T\right) / 1000$ For $0.9 \%$ Aqueous Ethanol Solution.

| Temperature ${ }^{\circ} \mathrm{C}$. | $\mathrm{E} / \mathrm{R} \div 1000=-\mathrm{T}^{2}(\Delta \ln \nu / \Delta \mathrm{T}) / 1000$ |  |  | Temperature ${ }^{\circ} \mathrm{C}$. | $\mathrm{E} / \mathrm{R} \div 1000=-\mathrm{T}^{2}(\Delta \ln \nu / \Delta \mathrm{T}) / 1000$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Heating sequence | Cooling sequence | $\begin{gathered} \text { Mean } E / R \div \\ 1000 \end{gathered}$ |  | Heating sequence | Cooling sequence | $\begin{gathered} \text { Mean } E / R \div \\ 1000 \end{gathered}$ |
| 10.50 | $2.306 \pm 0.003$ | $2.313 \pm 0.003$ | $2.310 \pm 0.003$ | 35.50 | $1.901 \pm 0.004$ | $1.912 \pm 0.004$ | $1.906 \pm 0.006$ |
| 11.50 | $2.294 \pm 0.003$ | $2.305 \pm 0.003$ | $2.300 \pm 0.005$ | 36.50 | $1.803 \pm 0.004$ | $1.796 \pm 0.004$ | $1.799 \pm 0.003$ |
| 12.50 | $2.298 \pm 0.003$ | $2.292 \pm 0.003$ | $2.295 \pm 0.003$ | 37.50 | $1.802 \pm 0.004$ | $1.809 \pm 0.004$ | $1.806 \pm 0.004$ |
| 13.50 | $2.317 \pm 0.003$ | $2.302 \pm 0.003$ | $2.310 \pm 0.008$ | 38.50 | $1.816 \pm 0.004$ | $1.805 \pm 0.004$ | $1.811 \pm 0.006$ |
| 14.50 | $2.206 \pm 0.003$ | $2.213 \pm 0.003$ | $2.210 \pm 0.003$ | 39.50 | $1.783 \pm 0.004$ | $1.792 \pm 0.004$ | $1.788 \pm 0.004$ |
| 15.50 | $2.204 \pm 0.003$ | $2.207 \pm 0.003$ | $2.205 \pm 0.002$ | 40.50 | $1.769 \pm 0.005$ | $1.764 \pm 0.005$ | $1.767 \pm 0.003$ |
| 16.50 | $2.218 \pm 0.003$ | $2.231 \pm 0.003$ | $2.225 \pm 0.007$ | 41.50 | $1.775 \pm 0.005$ | $1.783 \pm 0.005$ | $1.779 \pm 0.004$ |
| 17.50 | $2.186 \pm 0.003$ | $2.176 \pm 0.003$ | $2.181 \pm 0.005$ | 42.50 | $1.789 \pm 0.005$ | $1.782 \pm 0.005$ | $1.786 \pm 0.003$ |
| 18.50 | $2.073 \pm 0.003$ | $2.080 \pm 0.003$ | $2.076 \pm 0.004$ | 43.50 | $1.782 \pm 0.005$ | $1.779 \pm 0.005$ | $1.881 \pm 0.003$ |
| 19.50 | $2.103 \pm 0.003$ | $2.098 \pm 0.003$ | $2.100 \pm 0.003$ | 44.50 | $1.723+0.005$ | $1.736 \pm 0.005$ | $1.729 \pm 0.004$ |
| 20.50 | $2.092 \pm 0.004$ | $2.097 \pm 0.004$ | $2.094 \pm 0.003$ | 45.50 | $1.730-0.004$ | $1.717 \pm 0.004$ | $1.723 \pm 0.007$ |
| 21.50 | $2.116 \pm 0.004$ | $2.103 \pm 0.004$ | $2.109 \pm 0.007$ | 46.50 | $1.725 \pm 0.004$ | $1.734 \pm 0.004$ | $1.729 \pm 0.005$ |
| 22.50 | $2.101 \pm 0.004$ | $2.109 \pm 0.004$ | $2.105 \pm 0.004$ | 47.50 | $1.731 \pm 0.004$ | $1.739 \pm 0.004$ | $1.735 \pm 0.004$ |
| 23.50 | $2.072 \pm 0.004$ | $2.078 \pm 0.004$ | $2.075 \pm 0.003$ | 48.50 | $1.726 \pm 0.004$ | $1.714 \pm 0.004$ | $1.720 \pm 0.006$ |
| 24.50 | $1.996 \pm 0.004$ | $1.983 \pm 0.004$ | $1.990 \pm 0.006$ | 49.50 | $1.730 \pm 0.004$ | $1.739 \pm 0.004$ | $1.334 \pm 0.004$ |
| 25.50 | $2.006 \pm 0.004$ | $1.995 \pm 0.004$ | $2.001 \pm 0.005$ | 50.50 | $1.638 \pm 0.005$ | $1.626 \pm 0.005$ | $1.632 \pm 0.004$ |
| 26.50 | $1.999 \pm 0.004$ | $2.009 \pm 0.004$ | $2.004 \pm 0.005$ | 51.50 | $1.600 \pm 0.005$ | $1.609 \pm 0.005$ | $1.605 \pm 0.005$ |
| 27.50 | $2.000 \pm 0.004$ | $1.993 \pm 0.004$ | $1.997 \pm 0.003$ | 52.50 | $1.601 \pm 0.005$ | $1.610 \pm 0.005$ | $1.606 \pm 0.005$ |
| 28.50 | $1.987 \pm 0.004$ | $1.994 \pm 0.004$ | $1.991 \pm 0.004$ | 53.50 | $1.609 \pm 0.005$ | $1.602 \pm 0.005$ | $1.606 \pm 0.004$ |
| 29.50 | $2.003 \pm 0.004$ | $1.998 \pm 0.004$ | $2.001 \pm 0.003$ | 54.50 | $1.634 \pm 0.005$ | $1.619 \pm 0.005$ | $1.627 \pm 0.008$ |
| 30.50 | $1.999 \pm 0.005$ | $1.990 \pm 0.005$ | $1.995 \pm 0.005$ | 55.50 | $1.609 \pm 0.005$ | $1.600 \pm 0.005$ | $1.604 \pm 0.004$ |
| 31.50 | $1.894 \pm 0.005$ | $1.905 \pm 0.005$ | $1.899 \pm 0.006$ | 56.50 | $1.570 \pm 0.005$ | $1.584 \pm 0.005$ | $1.577 \pm 0.006$ |
| 32.50 | $1.903 \pm 0.005$ | $1.897 \pm 0.005$ | $1.900 \pm 0.003$ | 57.50 | $1.632 \pm 0.005$ | $1.619 \pm 0.005$ | $1.625 \pm 0.007$ |
| 33.50 | $1.893 \pm 0.005$ | $1.908 \pm 0.005$ | $1.901 \pm 0.007$ | 58.50 | $1.554 \pm 0.005$ | $1.567 \pm 0.005$ | $1.561 \pm 0.006$ |
| 34.50 | $1.904 \pm 0.005$ | $1.896 \pm 0.005$ | $1.900 \pm 0.004$ | 59.50 | $1.507 \pm 0.005$ | $1.513 \pm 0.005$ | $1.510 \pm 0.003$ |



Fig. 2.-Plots of E/R 1000 against temperature for various concentrations of ethanol solutions, each shifted 0.1 unit upwards above the lower concentration. The scale is correct for the broken-line curve in the middle of the figure, which represents $2.5 \%$ solutions of the earlier data. The lowest full-line curve for pure water (i.e. $0 \%$ ethanol) is also reproduced from the earlier work, and the curve drawn through the solid circles, shifted 0.1 unit above this, is for $0.9 \%$ ethanol, while that through the triangles and shifted 0.2 units above the curve for water is for $1.8 \%$ ethanol solutions.

The curve for $3.5 \%$ ethanol is drawn through the hollow circles, while that through the crosses $(0.1$ unit above this) is the curve for $4.1 \%$ alcohol solution. The curve for $5 \%$ ethanol from the earlier work is indicated by the full-line at the top (shifted 0.3 units above that for $2.5 \%$ solution).

Table I (b) shows the measured values for I. $8 \%$ solutions, both for heating and cooling sequences against the temperature and their standard deviation. These En values also have an r.m.s. scatter of the order of $\pm 0.005$ units and are plotted as triangles (shifted up o.r above the curve for $0.9 \%$ alcohol). Each of these steps extends over approximately $4.0^{\circ} \mathrm{C}$., with average drop of 0.07
unit of (E/R)/1000 between steps. We may conjecture that this decrease in the temperature interval is due to appearance of certain sub-steps. The movement of some of the main steps can be readily traced in Fig. 2 from pure water through $0.9 \%$ and $\mathrm{I} .8 \%$ upto $2.5 \%$ ethanol for which the broken line graph is plotted one unit above that for $1.8 \%$.

Table i(b).-Measured Agtivation Energies $\mathrm{E} / \mathrm{R} \div$ iooo $=-\mathrm{T}^{2}(\Delta \ln v / \Delta \mathrm{T}) / \mathrm{Iooo}$ for 1. $8 \%$ Aqueous Ethanol Solutions, in the Range of io to $51{ }^{\circ} \mathrm{C}$.

| Temperature ${ }^{\circ} \mathrm{C}$. | $\mathrm{E} / \mathrm{R} \div 1000=-\mathrm{T}^{2}(\Delta \ln \varphi / \Delta \mathrm{T}) / 1000$ |  |  | Temperature ${ }^{\circ} \mathrm{C}$. | $\mathrm{E} / \mathrm{R} \div 1000=-\mathrm{T}^{2}(\Delta \ln \nu / \Delta \mathrm{T}) / 1000$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Heating sequence | Cooling sequence | Overall mean |  | Heating sequence | Cooling sequence | Overall mean |
| 10.50 | $2.380 \pm 0.003$ | $2.368 \pm 0.003$ | $2.374 \pm 0.006$ | 31.50 | $2.019 \pm 0.005$ | $2.010 \pm 0.005$ | $2.015 \pm 0.005$ |
| 11.50 | $2.400 \pm 0.003$ | $2.407 \pm 0.003$ | $2.403 \pm 0.004$ | 32.50 | $1.941 \pm 0.005$ | $1.930 \pm 0.005$ | $1.935 \pm 0.005$ |
| 12.50 | $2.326 \pm 0.003$ | $2.318 \pm 0.003$ | $2.322 \pm 0.004$ | 33.50 | $1.860 \pm 0.005$ | $1.869 \pm 0.005$ | $1.865 \pm 0.004$ |
| 13.50 | $2.322 \pm 0.003$ | $2.321 \pm 0.003$ | $2.322 \pm 0.001$ | 34.50 | $1.868 \pm 0.005$ | $1.879 \pm 0.005$ | $1.874 \pm 0.005$ |
| 14.50 | $2.329 \pm 0.003$ | $2.320 \pm 0.003$ | $2.325 \pm 0.004$ | 35.50 | $1.886 \pm 0.005$ | $1.877 \pm 0.005$ | $1.882 \pm 0.005$ |
| 15.50 | $2.268 \pm 0.005$ | $2.361 \pm 0.005$ | $2.365 \pm 0.003$ | 36.50 | $1.871 \pm 0.005$ | $1.861 \pm 0.005$ | $1.866 \pm 0.005$ |
| 16.50 | $2.252 \pm 0.005$ | $2.258 \pm 0.005$ | $2.255 \pm 0.003$ | 37.50 | $1.864 \pm 0.005$ | $1.859 \pm 0.005$ | $1.861 \pm 0.003$ |
| 17.50 | $2.246 \pm 0.005$ | $2.233 \pm 0.005$ | $2.240 \pm 0.007$ | 38.50 | $1.837 \pm 0.005$ | $1.824 \pm 0.005$ | $1.831 \pm 0.007$ |
| 18.50 | $2.197 \pm 0.005$ | $2.204 \pm 0.005$ | $2.201 \pm 0.003$ | 39.50 | $1.819 \pm 0.005$ | $1.810 \pm 0.005$ | $1.815 \pm 0.005$ |
| 19.50 | $2.209 \pm 0.005$ | $2.201 \pm 0.005$ | $2.205 \pm 0.004$ | 40.50 | $1.815 \pm 0.006$ | $1.807 \pm 0.006$ | $1.811 \pm 0.004$ |
| 20.50 | $2.228 \pm 0.004$ | $2.213 \pm 0.004$ | $2.220 \pm 0.007$ | 41.50 | $1.826 \pm 0.006$ | $1.815 \pm 0.006$ | $1.822 \pm 0.006$ |
| 21.50 | $2.179 \pm 0.004$ | $2.172 \pm 0.004$ | $2.176 \pm 0.003$ | 42.50 | $1.824 \pm 0.006$ | $1.820 \pm 0.006$ | $1.822 \pm 0.002$ |
| 22.50 | $2.136 \pm 0.004$ | $2.125 \pm 0.004$ | $2.131 \pm 0.005$ | 43.50 | $1.725 \pm 0.006$ | $1.736 \pm 0.006$ | $1.730 \pm 0.006$ |
| 23.50 | $2.091 \pm 0.004$ | $2.080 \pm 0.004$ | $2.086 \pm 0.006$ | 44.50 | $1.736 \pm 0.006$ | $1.729 \pm 0.006$ | $1.733 \pm 0.004$ |
| 24.50 | $2.103 \pm 0.004$ | $2.100 \pm 0.004$ | $2.102 \pm 0.002$ | 45.50 | $1.748 \pm 0.006$ | $1.731 \pm 0.006$ | $1.740 \pm 0.008$ |
| 25.50 | $2.056 \pm 0.006$ | $2.058 \pm 0.006$ | $2.057 \pm 0.002$ | 46.50 | $1.726 \pm 0.006$ | $1.713 \pm 0.006$ | $1.720 \pm 0.007$ |
| 26.50 | $2.066 \pm 0.006$ | $2.061 \pm 0.006$ | $2.063 \pm 0.003$ | 47.50 | $1.755 \pm 0.006$ | $1.746 \pm 0.006$ | $1.751 \pm 0.006$ |
| 27.50 | $2.073 \pm 0.006$ | $2.054 \pm 0.006$ | $2.068 \pm 0.004$ | 48.50 | $1.742 \pm 0.006$ | $1.740 \pm 0.006$ | $1.741 \pm 0.002$ |
| 28.50 | $2.077 \pm 0.006$ | $2.065 \pm 0.006$ | $2.071 \pm 0.006$ | 49.50 | $1.729 \pm 0.006$ | $1.730 \pm 0.006$ | $1.730 \pm 0.001$ |
| 29.50 | $1.988 \pm 0.005$ | $1.981 \pm 0.005$ | $1.985 \pm 0.004$ | 50.50 |  |  |  |
| 30.50 | $2.006 \pm 0.005$ | $1.995 \pm 0.005$ | $2.015 \pm 0.006$ |  |  |  |  |

Note.-The deviations quoted with the overall means are half the differences between the values of $\mathrm{E} / \mathrm{R} \div 1000$ for the heating and cooling sequences.

## Results with $3 \cdot 5 \%$ and $4 \cdot 1 \%$ Ethanol

To further trace out the movements of the energy jumps over the large gap between the previously reported data for solutions of $2.5 \%$ and $5 \%$ alcohol concentration, it was considered desirable to examine two more solutions in this concentration range. Aqueous ethanol of $3.5 \%$ and $4.1 \%$ concentration was prepared and used for the viscosity measurements with a thermal interval of $\mathrm{I}^{\circ} \mathrm{C}$. and the usual precautions, particularly against the evaporation of the test liquid. The flow activation energy values for the $3 \cdot 5 \%$ ethanol solution, both for heating and cooling sequences, together with their r.m.s. deviations (estimated from those of flow time and temperature), are given in Table 2(a). The curve drawn through hollow circles represents the mean values of $\mathrm{E} / \mathrm{R} \div$ 1000 for $3.5 \%$ dilute ethanol solution on vertical scale shifted o.I unit above $2.5 \%$ solution, while that shifted 0.2 units above through the corsses represents the $4.1 \%$ ethanol solution, both performed in the range of $7^{\circ} \mathrm{C}$. to $60^{\circ} \mathrm{C}$. The average step length is $4.4^{\circ} \mathrm{C}$. and $3.7^{\circ} \mathrm{C}$. with the mean drop of 0.08 and 0.075 units of (E/R)/1000.

Table 2(b) gives the Beckmann reading, corrected time of flow, mean temperature and calculated $(\mathrm{E} / \mathrm{R}) / \mathrm{I} 000$ values, together with their r.m.s. deviation (of the order of $\pm 0.006$ ) for $4.1 \%$ ethanol. For comparison purposes, the graph for $5,0 \%$ ethanol is reproduced from the earlier data and is represented, shifted o.I unit above 4. $1 \%$ graph, by the full line in the top of Fig. 2.

## Discussion

For understanding the exact course of the movements of the energy transition, as a function of concentration, a brief synopsis is given in Table 3. This Table gives the temperature at the various energy jumps or transitions, and their depths in terms of $(E / R) /$ rooo. This covers the range of $0 \%$ to $5 \%$ ethanol concentration and the various jumps are classified as "large" "medium" or "small", using the mean value of $\frac{\Delta \mathrm{E}}{\mathrm{R}} / \mathrm{r} 000=0.07$. A plot of the temperatures at the jumps for these solutions versus the concentration is given in Fig. 3, where the circles stand for large jumps, triangles for medium, and crosses for small ones.

Tabje 2(a).-Measured Activation Energies $\mathrm{E} / \mathrm{R} \div 1000=-\mathrm{T}^{2}(\Delta \ln \nu / \Delta \mathrm{T}) / \mathrm{I} 000$ for $3.5 \% \mathrm{w} / \mathrm{w}$ Aqueous Ethanol Solution in the Range of $7^{\circ} \mathrm{C}$ to $59^{\circ} \mathrm{C}$.

| Temperature ${ }^{\circ} \mathrm{C}$. | $\left.\mathrm{E} / \mathrm{R} \div 1000=-\mathrm{T}^{2}(\Delta \ln \nu / \Delta \mathrm{T})\right) / 1000$ |  |  |  | $\mathrm{E} / \mathrm{R} \div 1000=-\mathrm{T}^{2}(\Delta \ln v / \Delta \mathrm{T})$ |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | Heating <br> sequence | Cooling sequence | Overall mean | ture ${ }^{\circ} \mathrm{C}$. | Heating sequence | Cooling sequence | Overall mean |
| 7.50 | $2.605 \pm 0.004$ | $2.601 \pm 0.004$ | $2.603 \pm 0.003$ | 33.50 | $2.095 \pm 0.003$ | $2.086 \pm 0.003$ | $2.091 \pm 0.005$ |
| 8.50 | $2.631 \pm 0.004$ | $2.618 \pm 0.004$ | $2.625 \pm 0.007$ | 34.50 | $1.983 \pm 0.003$ | $1.980 \pm 0.003$ | $1.981 \pm 0.002$ |
| 9.50 | $2.600 \pm 0.004$ | $2.594 \pm 0.004$ | $2.597 \pm 0.003$ | 35.50 | $1.990 \pm 0.003$ | $1.981 \pm 0.003$ | $1.986 \pm 0.005$ |
| 10.50 | $2.531 \pm 0.004$ | $2.519 \pm 0.004$ | $2.525 \pm 0.006$ | 36.50 | $1.993 \pm 0.003$ | $1.987 \pm 0.003$ | $1.990 \pm 0.003$ |
| 11.50 | $2.547 \pm 0.004$ | $2.544 \pm 0.004$ | $2.546 \pm 0.002$ | 37.50 | $1.993 \pm 0.004$ | $1.986 \pm 0.004$ | $1.990 \pm 0.004$ |
| 12.50 | $2.460 \pm 0.004$ | $2.451 \pm 0.004$ | $2.456 \pm 0.005$ | 38.50 | $2.002 \pm 0.004$ | $2.000 \pm 0.004$ | $2.001 \pm 0.001$ |
| 13.50 | $2.416 \pm 0.004$ | $2.425 \pm 0.004$ | $2.421 \pm 0.004$ | 39.50 | $1.913 \pm 0.004$ | $1.908 \pm 0.004$ | $1.910 \pm 0.002$ |
| 14.50 | $2.427 \pm 0.004$ | $2.434 \pm 0.004$ | $2.430 \pm 0.003$ | 40.50 | $1.916 \pm 0.004$ | $1.907 \pm 0.004$ | $1.912 \pm 0.005$ |
| 15.50 | $2.421 \pm 0.004$ | $2.428 \pm 0.004$ | $2.425 \pm 0.003$ | 41.50 | $1.923 \pm 0.005$ | $1.928 \pm 0.005$ | $1.926 \pm 0.003$ |
| 16.50 | $2.378 \pm 0.004$ | $2.371 \pm 0.004$ | $2.375 \pm 0.004$ | 42.50 | $1.908 \pm 0.005$ | $1.901 \pm 0.005$ | $1.905 \pm 0.004$ |
| 17.50 | $2.313 \pm 0.004$ | $2.311 \pm 0.004$ | $2.312 \pm 0.001$ | 43.50 | $1.937 \pm 0.005$ | $1.922 \pm 0.005$ | $1.929 \pm 0.007$ |
| 18.50 | $2.330 \pm 0.004$ | $2.320 \pm 0.004$ | $2.325 \pm 0.005$ | 44.50 | $1.927 \pm 0.005$ | $1.923 \pm 0.005$ | $1.925 \pm 0.002$ |
| 19.50 | $2.301 \pm 0.004$ | $2.291 \pm 0.004$ | $2.296 \pm 0.005$ | 45.50 | $1.868 \pm 0.004$ | $1.872 \pm 0.004$ | $1.870 \pm 0.002$ |
| 20.50 | $2.313 \pm 0.005$ | $2.311 \pm 0.005$ | $2.312 \pm 0.001$ | 46.50 | $1.884 \pm 0.004$ | $1.877 \pm 0.004$ | $1.881 \pm 0.004$ |
| 21.50 | $2.307 \pm 0.005$ | $2.298 \pm 0.005$ | $2.303 \pm 0.004$ | 47.50 | $1.867 \pm 0.004$ | $1.869 \pm 0.004$ | $1.868 \pm 0.001$ |
| 22.50 | $2.318 \pm 0.005$ | $2.311 \pm 0.005$ | $2.315 \pm 0.004$ | 48.50 | $1.786 \pm 0.004$ | $1.775 \pm 0.004$ | $1.781 \pm 0.006$ |
| 23.50 | $2.203 \pm 0.005$ | $2.201 \pm 0.005$ | $2.202 \pm 0.001$ | 49.50 | $1.784 \pm 0.004$ | $1.777 \pm 0.004$ | $1.780 \pm 0.004$ |
| 24.50 | $2.216 \pm 0.005$ | $2.205 \pm 0.005$ | $2.211 \pm 0.006$ | 50.50 | $1.788 \pm 0.004$ | $1.781 \pm 0.004$ | $1.785 \pm 0.004$ |
| 25.50 | $2.170 \pm 0.003$ | $2.161 \pm 0.003$ | $2.166 \pm 0.005$ | 41.50 | $1.770 \pm 0.004$ | $1.781 \pm 0.004$ | $1.775 \pm 0.006$ |
| 26.50 | $2.183 \pm 0.003$ | $2.188 \pm 0.003$ | $2.185 \pm 0.003$ | 52.50 | $1.785 \pm 0.004$ | $1.780 \pm 0.004$ | $1.783 \pm 0.003$ |
| 27.50 | $2.185 \pm 0.003$ | $2.180 \pm 0.003$ | $2.182 \pm 0.003$ | 53.50 | $1.775 \pm 0.004$ | $1.774 \pm 0.004$ | $1.775 \pm 0.001$ |
| 28.50 | $2.193 \pm 0.003$ | $2.187 \pm 0.003$ | $2.190 \pm 0.003$ | 54.50 | $1.700 \pm 0.004$ | $1.692 \pm 0.004$ | $1.696 \pm 0.004$ |
| 29.50 | $2.099 \pm 0.003$ | $2.090 \pm 0.003$ | $2.094 \pm 0.005$ | 55.50 | $1.706 \pm 0.006$ | $1.656 \pm 0.006$ | $1.701 \pm 0.005$ |
| 30.50 | $2.086 \pm 0.003$ | $2.075 \pm 0.003$ | $2.081 \pm 0.006$ | 56.50 | $1.648 \pm 0.006$ | $1.661 \pm 0.006$ | $1.655 \pm 0.007$ |
| 31.50 | $2.088 \pm 0.003$ | $2.080 \pm 0.003$ | $2.084 \pm 0.004$ | 57.50 | $1.697 \pm 0.006$ | $1.704 \pm 0.006$ | $1.701 \pm 0.003$ |
| 32.50 | $2.077 \pm 0.003$ | $2.082 \pm 0.003$ | $2.080 \pm 0.002$ | 58.50 | $1.705 \pm 0.006$ | $1.697 \pm 0.006$ | $1.701 \pm 0.004$ |

Several of these plotted points can be definitely linked together, as represented by the full lines, while other involve some ambiguity, and are


Fig. 3.- Chart showing the position of the jumps in the flow activation energy for several ethanol concentrations in the range of $0 \%$ to $5 \%$ ethanol. The various jumps are classified as large, medium or small (compared with the mean value of $\Delta(\mathrm{E} / \mathrm{R}) / 1000$ $=0.07$ ), and are plotted as circles, triangles and crosses, respectively. The full lines connecting some of the plotted points indicate the more or less definite movements of these jumps, and the broken lines stand for those parts involving some ambiguity. The dotted lines show the possible course of the jumps in two regions where the data is not available at present. Several new branches appear to develop in this chart.
joined by broken lines. In two regions, where part of the data is not available so far, the probable course of the jumps is indicated by dotted lines.

A careful examination of this plot shows that the shift of these jumps with changes in concentration is mostly smooth in character, in agreement with the idea advanced earlier, but does not always follow the pattern in Fig. I based on the results of the previous communications. Two facts are clear; firstly, there is appearance and disappearance of certain steps accompanied by changes in the magnitude of the jump; secondly, the phenomena are rather complex in some regions where branching of the discontinuities with the variation of alcohol concentration takes place, particularly at the temperatures around $30^{\circ} \mathrm{C}$. For instance, the jump in $0 \%$ (i.e. water) at $22.0^{\circ} \mathrm{C}$. and $27.4^{\circ} \mathrm{C}$. are branched with $0.9 \%$ solutions at $23.8^{\circ} \mathrm{C}$. and $30.6^{\circ} \mathrm{C}$. respectively. The two branches of first jump are going normally up to $5 \%$ ethanol, while for the second jump one branch goes more or less straight near $29^{\circ} \mathrm{C}$. and the other is further branched at $2.5 \%$ solutions.

Table 2 (b).—Beckmann Readings, Flow Times and the Caloulated Values of $(\mathrm{E} / \mathrm{R}) / \mathrm{rooo}=-\mathrm{T}^{2}(\Delta \ln v / \Delta \mathrm{T}) / \mathrm{I}$ ooo for $4.1 \%$ Aqueous Ethanol in the Range of $8^{\circ} \mathrm{C}$. to $61^{\circ} \mathrm{C}$.

| Heating sequence |  |  |  |  |  | Cooling sequence |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Temperature "C. | Beckniann reading | Time of flow corrected for level | Mean temperature. ${ }^{\circ} \mathrm{C}$. | $\overbrace{$ Uncorr  <br>  ted }$^{\mathrm{E} / \mathrm{R}}$ | $\frac{1000}{\text { rec- }} \begin{gathered} \text { Correc- } \\ \text { ted } \end{gathered}$ | Temperature ${ }^{\circ} \mathrm{C}$. | Beckmann reading | Time of flow corrected for level | Mean tempe-rature${ }^{\circ} \mathrm{C}$. |  | $\frac{1000}{2 \div 1000}$ | $\begin{gathered} \text { Mean } \\ \mathrm{E} / \mathrm{R} \div 1000 \end{gathered}$ |
| 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 |
| 8.0 | $3.762 \pm 0.000$ | $446.21 \pm 0.01$ |  |  |  | 8.0 | $3.761 \pm 0.000$ | $446.08 \pm 0.01$ |  |  |  |  |
| 9.0 | $2.761 \pm 0.000$ | $431.64 \pm 0.02$ | 8.50 | 2.630 | $2.625 \pm 0.003$ | 9.0 | $2.762 \pm 0.001$ | $431.59 \pm 0.01$ | 8.50 | 2.622 | $2.617 \pm 0.003$ | $2.621 \pm 0.004$ |
|  |  |  | 9.50 | 2.650 | $2.648 \pm 0.003$ |  |  |  | 9.50 | 2.634 | $2.632 \pm 0.003$ | $2.640 \pm 0.008$ |
| 10.0 | $1.762 \pm 0.001$ | $417.57 \pm 0.01$ | 10.50 | 2.626 |  | 10.0 | $1.761 \pm 0.001$ | $417.59 \pm 0.02$ | 10.50 | 2.634 |  |  |
| 11.0 | $0.761 \pm 0.001$ | $404.15 \pm 0.02$ |  |  |  | 11.0 | $0.762 \pm 0.000$ | $404.15 \pm 0.01$ |  |  |  |  |
| 11.0 | $4.072 \pm 0.000$ | $404.42 \pm 0.01$ |  |  |  | 11.0 | $4.076 \pm 0.000$ | $403.40 \pm 0.01$ |  |  |  |  |
|  |  |  | 11.50 | 2.517 | $2.521 \pm 0.005$ |  |  |  | 11.50 | 2.532 | $2.536 \pm 0.005$ | $2.528 \pm 0.008$ |
| 12.0 | $3.072 \pm 0.001$ | $392.05 \pm 0.02$ | 12.50 | 2.518 | $2.513 \pm 0.005$ | 12.0 | $3.072 \pm 0.001$ | $391.91 \pm 0.02$ | 12.50 | 2.535 | $2.530 \pm 0.005$ | $2.521 \pm 0.009$ |
| 13.0 | $2.072 \pm 0.000$ | $380.14 \pm 0.01$ |  |  |  | 13.0 | $2.076 \pm 0.000$ | $379.97 \pm 0.01$ |  |  |  |  |
|  |  |  | 13.50 | 2.522 | $2.520 \pm 0.005$ |  |  |  | 13.50 | 2.525 | $2.523 \pm 0.005$ | $2.521 \pm 0.002$ |
| 14.0 | 1. | 36 | 14.50 | 2.476 | $2.473 \pm 0.005$ |  |  | $368.45 \pm 0.02$ | 14.50 | 2.466 | $2.463 \pm 0.005$ | $2.468 \pm 0.005$ |
| 15.0 | $0.072 \pm 0.000$ | $357.70 \pm 0.01$ |  |  |  | 15.0 | $0.073 \pm 0.000$ | $357.62 \pm 0.01$ |  |  |  |  |
| 15.0 | $3.646 \pm 0.000$ | $356.64 \pm 0.01$ |  |  |  | 15.0 | $3.646 \pm 0.000$ | $356.56 \pm 0.02$ |  |  |  |  |
|  |  |  | 15.5 | 2.491 | $2.491 \pm 0.005$ |  |  |  | 15.50 | 2.478 | $2.478 \pm 0.005$ | $2.485 \pm 0.006$ |
| 16.0 | $2.647 \pm 0.001$ | $346.16 \pm 0.01$ | 16.50 | 2.469 | $2.470+0.005$ | 16.0 | $2.647 \pm 0.000$ | $346.12 \pm 0.01$ | 16.50 | 2.465 | $2.466+0.005$ | $2.468 \pm 0.002$ |
| 17.0 | $1.647 \pm 0.000$ | $336.12 \pm 0.01$ |  |  |  | 17.0 | $1.647 \pm 0.001$ | $336.10 \pm 0.02$ |  |  |  |  |
| 18.0 | $0.647 \pm 0.001$ | $326.81 \pm 0.02$ | 17.50 | 2.373 | $2.373=0.005$ | 18.0 | $0.646 \pm 0.000$ | $326.72 \pm 0.02$ | 17.5 | 2.389 | $2.389 \pm 0.005$ | $2.381 \pm 0.008$ |
| 18.0 | $5.041 \pm 0.001$ | $327.54 \pm 0.01$ |  |  |  | 18.0 | $5.042 \pm 0.000$ | $327.41 \pm 0.01$ |  |  |  |  |
|  |  |  | 18.50 | 2.377 | $2.382 \pm 0.005$ |  |  |  | 18.50 | 2.373 | $2.378 \pm 0.005$ | $2.380 \pm 0.008$ |
| 19.0 | $4.042 \pm 0.000$ | $318.52 \pm 0.01$ | 19.50 | 2.321 | $2.321+0.005$ | 19.0 | $4.042 \pm 0.000$ | $318.41 \pm 0.01$ | 19.50 | 2.313 | $2.313+0.005$ | $2.317+0.004$ |
| 20.0 | $3.042 \pm 0.001$ | $310.00 \pm 0.00$ |  |  |  | 20.0 | $3.043 \pm 0.000$ | $309.94 \pm 0.02$ |  |  |  |  |
|  |  |  | 20.50 | 2.285 | $2.285 \pm 0.005$ |  |  |  | 20.50 | 2.297 | $2.297 \pm 0.005$ | $2.291 \pm 0.006$ |
| 21.0 | $2.042 \pm 0.000$ | $301.89 \pm 0.01$ |  |  |  | 21.0 | $2.043 \pm 0.000$ | $301.80 \pm 0.01$ |  |  |  | $2.290+0.004$ |
| 22.0 | $1.042 \pm 0.000$ | $294.04 \pm 0.02$ | 21.50 | 2.286 | $2.286 \pm 0.005$ | 22.0 | $1.041 \pm 0.000$ | $293.92 \pm 0.01$ | 21.50 | 2.294 | $2.294 \pm 0.005$ | $2.290 \pm 0.004$ |
| 22.0 | $4.383 \pm 0.000$ | $293.42 \pm 0.01$ |  |  |  | 22.0 | $4.382 \pm 0.000$ | $293.49 \pm 0.01$ |  |  |  |  |
| 23. | 3 |  | 22.50 | 2.255 | $2.254 \pm 0.003$ | 23 |  | $28$ | 22.50 | 2.247 | $2.246 \pm 0.003$ | $2.250 \pm 0.004$ |


| 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  | 23.50 | 2.272 | $2.269 \pm 0.003$ |  |  |  | 23.50 | 2.260 | $2.257 \pm 0.003$ | $2.263 \pm 0.006$ |
| . 0 | $2.355 \pm 0.000$ | $278.46 \pm 0.00$ | 24.50 | 2.242 | $2.244 \pm 0.003$ | 24.0 | $2.355 \pm 0.001$ | $278.60 \pm 0.00$ | 24.50 | 2.254 | $2.256 \pm 0.003$ | $2.250 \pm 0.006$ |
| 25.0 | $1.355 \pm 0.000$ | $271.50 \pm 0.01$ |  |  |  | 25.0 | $1.355 \pm 0.001$ | $271.60 \pm 0.01$ |  |  |  |  |
| 26.0 | $0.354 \pm 0.001$ | $264.69 \pm 0.00$ | 25.50 | 2.263 | $2.263 \pm 0.003$ | 26.0 | $0.355 \pm 0.000$ | $264.81 \pm 0.01$ | 25.50 | 2.258 | $2.258 \pm 0.003$ | $260 \pm 0.003$ |
| 26.0 | $5.045 \pm 0.001$ | $264.86 \pm 0.01$ |  |  |  | 26.0 | $5.044 \pm 0.001$ | $265.35 \pm 0.01$ |  |  |  |  |
| 27.0 | $4.045 \pm 0.000$ | $258.57 \pm 0.01$ | 26.50 | 2.158 | $2.160 \pm 0.005$ | 27.0 | $4.044 \pm 0.000$ | $259.02 \pm 0.01$ | 26.5 | 2.168 | $2.170 \pm 0.005$ | $2.165 \pm 0.005$ |
|  |  |  | 27.50 | 2.184 | $2.179 \pm 0.005$ |  |  |  | 27.50 | 2.194 | $2.189 \pm 0.005$ | $2.184 \pm 0.005$ |
| 28.0 | $3.045 \pm 0.000$ | $252.41 \pm 0.01$ | 28.50 | 2.169 | $2.163 \pm 0.005$ | 28.0 | $3.044 \pm 0.00$ | $252.81 \pm 0.01$ | 28.50 | 2.177 | $2.171 \pm 0.005$ | $2.167 \pm 0.004$ |
| 29.0 | $2.043 \pm 0.001$ | $246.46 \pm 0.00$ |  | 2.180 | $2.186+0.005$ | 29.0 | $2.045 \pm 0.000$ | $246.84 \pm 0.00$ | 29.50 | 2.172 | $2.178+0.005$ | $2.182+0.004$ |
| 30.0 | $1.045 \pm 0.000$ | $240.69 \pm 0.00$ |  |  |  | 30.0 | $1.042 \pm 0.001$ | $244.04 \pm 0.01$ |  |  |  |  |
| 30.0 | $4.699 .0 \pm 001$ | $241.06 \pm 0.01$ |  |  |  | 30.0 | $4.696 \pm 0.001$ | $240.79 \pm 0.01$ |  |  |  |  |
| 31.0 | $3.698 \pm 0.000$ | $235.63 \pm 0.00$ | 30.50 | 2.100 |  | 31.0 | $3.696 \pm 0.001$ | $235.36 \pm 0.01$ | 30.50 | 2.103 | $2.103 \pm 0.006$ | $2.101 \pm 0.002$ |
|  |  |  | 31.50 | 2.119 | $2.114 \pm 0.006$ |  |  |  | 31.50 | 2.110 | $2.105 \pm 0.006$ | $2.110 \pm 0.005$ |
| 32.0 | $2.693 \pm 0.000$ | $230.29 \pm 0.01$ | 32.50 | 2.100 | $2.107 \pm 0.006$ | 32.0 | $2.694 \pm 0.000$ | $230.66 \pm 0.00$ | 32.50 | 2.119 | $2.116 \pm 0.006$ | $2.112 \pm 0.004$ |
| 33.0 | $1.699 \pm 0.000$ | $225.20 \pm 0.01$ | 33.50 | 2.054 | $2.059+0.006$ | 33.0 | $1.697 \pm 0.001$ | $224.94 \pm 0.01$ | 33.50 | 2.064 | $2.068+0.006$ |  |
| 34.0 | $0.698 \pm 0.001$ | $220.33 \pm 0.01$ |  |  |  | 34.0 | $0.698 \pm 0.000$ | $220.06 \pm 0.01$ |  |  |  |  |
| 34.0 | $4.546 \pm 0.000$ | $220.10 \pm 0.00$ |  |  |  | 34.0 | $4.546 \pm 0.000$ | $220.17 \pm 0.01$ |  |  |  |  |
| 35.0 | $3.544 \pm 0.000$ | $215.54 \pm 0.01$ | 34.50 | 1.981 | $1.981 \pm 0.006$ | 35.0 | $3.545 \pm 0.001$ | $215.63 \pm 0.01$ | 34.50 | 1.970 | $1.970 \pm 0.006$ | $1.976 \pm 0.006$ |
|  |  |  | 35.50 | 1.983 | $1.983 \pm 0.006$ |  |  |  | 35.50 | 1.991 | $1.991 \pm 0.006$ | $1.987 \pm 0.004$ |
| 36.0 | $2.546 \pm 0.001$ | $211.11 \pm 0.01$ | 36.50 | 1.983 | $1.983 \pm 0.006$ | 36.0 | $2.545 \pm 0.000$ | $211.17 \pm 0.00$ | 36.50 | 1.977 | $1.977+0.006$ | $1.980+0.003$ |
| 37.0 | $1.546 \pm 0.000$ | $206.79 \pm 0.60$ | 37.50 | 1.993 | $1.997+0.006$ | 37.0 | $1.547 \pm 0.000$ | $206.87 \pm 0.00$ |  |  |  |  |
| 38.0 | $0.546 \pm 0.001$ | $262.56 \pm 0.01$ |  |  |  | 38.0 | $0.546 \pm 0.000$ | $202.67 \pm 0.01$ | 37.50 | 1.81 | $1.805 \pm 0.006$ | $1.91 \pm 0.006$ |
| 38.0 | $4.535+0.000$ | $202.92 \pm 0.01$ |  |  |  | 38.0 | $4.567 \pm 0.000$ | $203.17 \pm 0.00$ |  |  |  |  |
| 39.0 | $3.573 \pm 0.001$ | $198.96 \pm 0.01$ |  | 1.990 | $1.990 \pm 0.005$ | 39.0 | $3.567 \pm 0.001$ | $199.06 \pm 0.01$ | 38.50 | 1.984 | $1.984 \pm 0.005$ | $1.987 \pm 0.003$ |
|  |  |  | 39.50 | 1.990 | $1.987 \pm 0.005$ |  |  |  | 39.50 | 2.000 | $1.997 \pm 0.005$ | $1.992 \pm 0.006$ |
| 40.0 | $2.568 \pm 0.000$ | $194.97 \pm 0.00$ | 40.50 | 1.915 | $1.915+0.005$ | 40.0 | $2.567 \pm 0.000$ | $195.03 \pm 0.00$ | 40.50 | 1.905 | $1.905+0.005$ | $1.910+0.005$ |
| 41.0 | $1.568 \pm 0.001$ | $191.21 \pm 0.00$ |  |  | $1.95 \pm 0.05$ | 41.0 | $1.565 \pm 0.001$ | $191.29 \pm 0.01$ |  |  | . | $1.90 \pm 0.005$ |
| 42.0 | $0.571 \pm 0.000$ | $187.58 \pm 0.01$ | 41.50 | 1.908 | $1.906 \pm 0.005$ | 42.0 | $0.567 \pm 0.000$ | $187.51+0.00$ | 41.50 | 1.902 | $21.900 \pm 0.005$ | $1.903 \pm 0.003$ |


| 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 42.0 | $5.013 \pm 0.001$ | $187.60 \pm 0.01$ |  |  |  | 42.0 | $5.011 \pm 0.001$ | $187.46 \pm 0.01$ |  |  |  |  |
|  |  |  | 42.50 | 1.916 | $1.917 \pm 0.006$ |  |  |  | 42.50 | 1.903 | $1.905 \pm 0.006$ | $1.912 \pm 0.008$ |
| 43.0 | $4.012 \pm 0.000$ | $184.02 \pm 0.00$ | 43.50 | 1.900 | $1.900 \pm 0.006$ | 43.0 | $4.011 \pm 0.000$ | $183.91 \pm 0.00$ | 43.50 | 1.910 | $1.910 \pm 0.006$ | $1.905 \pm 0.005$ |
| 44.0 | $3.015 \pm 0.001$ | $180.57 \pm 0.01$ |  | 1. | $1.90 \pm 0.006$ | 44.0 | $3.011 \pm 0.001$ | $180.44 \pm 0.01$ | . 5 | 1.10 | $1.910 \pm 0.006$ | $1.905 \pm 0.005$ |
| 45.0 | 1.978 | 17 | 44.50 | 1.880 | $1.878 \pm 0.006$ | 45.0 | $1.978+0.000$ | $177.03+0.00$ | 44.50 | 1.866 | $1.864 \pm 0.006$ | $1.871 \pm 0.007$ |
|  |  |  | 45.50 | 1.880 | $1.884 \pm 0.006$ |  |  |  | 45.50 | 1.872 | $1.876 \pm 0.006$ | $1.880 \pm 0.04_{4}$ |
| 46.0 | $0.923 \pm 0.000$ | $173.69 \pm 0.01$ |  |  |  | 46.0 | $0.920 \pm 0.000$ | $173.61 \pm 0.01$ |  |  |  |  |
| 46.0 | $4.774 \pm 0.000$ | $173.46 \pm 0.00$ |  |  |  | 46.0 | $4.975 \pm 0.001$ | $173.40 \pm 0.01$ |  |  |  |  |
|  |  |  | 46.50 | 1.850 | $1.850 \pm 0.006$ |  |  |  | 46.50 | 1.840 | $1.840 \pm 0.006$ | $1.845 \pm 0.005$ |
| 47.0 | $3.929 \pm 0.001$ | $170.21 \pm 0.01$ | 47.50 | 1.824 |  | 47.0 | $3.936 \pm 0.000$ | $170.20 \pm 0.00$ | 47.50 | 1.816 |  | $1.819+0.004$ |
| 48.0 | $2.927 \pm 0.000$ | $167.21 \pm 0.01$ | 47.50 | 1.824 | $1.823 \pm 0.006$ | 48.0 | $2.919 \pm 0.001$ | $167.17 \pm 0.01$ | 47.50 | 1.816 | $1.815 \pm 0.006$ | $1.819 \pm 0.004$ |
| 49.0 |  |  | 48.50 | 1.840 | $1.837 \pm 0.006$ |  |  |  | 48.50 | 1.836 | $1.833 \pm 0.006$ | $1.835 \pm 0.002$ |
|  |  |  | 49.50 | 1.826 | $1.829 \pm 0.006$ |  |  |  | 49.50 | 1.818 | $1.821 \pm 0.006$ | $1.825 \pm 0.004$ |
| 50.0 | $0.841 \pm 0.000$ | $161.15 \pm 0.01$ |  |  |  | 50.0 | $0.843 \pm 0.001$ | $161.24 \pm 0.00$ |  |  |  |  |
| 50.0 | $5.036 \pm 0.001$ | $161.26 \pm 0.00$ |  |  |  | 50.0 | $5.035 \pm 0.000$ | $161.09 \pm 0.00$ |  |  |  |  |
|  |  |  | 50.50 | 1.812 | $1.817 \pm 0.008$ |  |  |  | 50.50 | 1.828 | $1.833 \pm 0.008$ | $1.825 \pm 0.008$ |
| 51.0 | $4.000 \pm 0.000$ | $158.40 \pm 0.01$ | 51.50 | 1.772 | $1.772 \pm 0.008$ | 51.0 | $3.999 \pm 0.001$ | $158.20 \pm 0.01$ | 51.50 | 1.776 | $1.776 \pm 0.008$ | $1.774 \pm 0.002$ |
| 52.0 | $2.937 \pm 0.002$ | $155.61 \pm 0.01$ |  |  |  | 52.0 | $2.935 \pm 0.000$ | $155.39 \pm 0.01$ |  |  |  |  |
| 53.0 | $1.878 \pm 0.000$ | $152.85 \pm 0.00$ | 52.50 | 1.792 | $1.792 \pm 0.008$ | 53.0 | $1.878 \pm 0.001$ | $152.66 \pm 0.01$ | 52.50 | 1.776 | $1.776 \pm 0.008$ | $1.784 \pm 0.008$ |
| 54.0 | $0.833 \pm 0.001$ | $150.20 \pm 0.00$ | 53.50 | 1.786 | $1.781 \pm 0.008$ | 54.0 | $0.843 \pm 0.000$ | $150.04 \pm 0.00$ | 53.50 | 1.780 | $1.775 \pm 0.008$ | $1.778 \pm 0.003$ |
| 54.0 | $5.208 \pm 0.002$ | $150.15 \pm 0.02$ | 54.50 | 1.780 |  | 54.0 | $5.205 \pm 0.001$ | $150.02 \pm 0.01$ | 54 | 1.772 | $1.776+0.008$ |  |
| 55.0 | $4.173 \pm 0.000$ | $147.60 \pm 0.00$ |  |  |  | 55.0 | $4.170 \pm 0.000$ | $147.48 \pm 0.00$ | 5 | 1.72 |  | $1.880 \pm 0.004$ |
| 56 | $3.139+0.001$ | $145.26+0.01$ | 55.50 | 1.669 | $1.664 \pm 0.008$ |  |  |  | 55.50 | 1.660 | $1.655 \pm 0.008$ | $1.660 \pm 0.005$ |
|  |  |  | 56.50 | 1.676 | $1.674 \pm 0.008$ |  |  |  | 56.50 | 1.670 | $1.668 \pm 0.008$ | $1.671 \pm 0.003$ |
| 57.0 | $2.069 \pm 0.000$ | $142.88 \pm 0.01$ | 57.50 | 1.635 |  | 57.0 | $2.074 \pm 0.001$ | $142.82 \pm 0.01$ | 57.50 | 1.634 | $1.639+0.008$ | $1.640+0.001$ |
| 58.0 | $1.000 \pm 0.001$ | $140.47 \pm 0.00$ |  |  |  | 58.0 | $1.000 \pm 0.000$ | $140.55 \pm 0 . C 0$ |  |  |  |  |
| 58.0 | $4.774 \pm 0.001$ | $141.77 \pm 0.00$ |  |  |  | 58.0 | $4.172 \pm 0.000$ | $141.71 \pm 0.00$ |  |  |  |  |
| 59.0 | $3.776 \pm 0.000$ | $139.63 \pm 0.01$ | 58.50 | 1.673 | $1.673 \pm 0.006$ | 59.0 | $3.775 \pm 0.001$ | $139.59+0.01$ | 58.50 | 1.661 | $1.661 \pm 0.006$ | $1.667 \pm 0.006$ |
|  |  |  | 59.50 | 1.665 | $1.665 \pm 0.006$ |  |  |  | 59.50 | 1.657 | $1.657 \pm 0.006$ | $1.661 \pm 0.004$ |
| 60.0 | $2.785 \pm 0.001$ | $137.56 \pm 0.00$ | 60.50 | 1.654 | $1.656+0.006$ | 60.0 | $2.774 \pm 0.000$ | $137.51 \pm 0.00$ | 60.50 | 1.664 | $1.666+000.6$ | $1.660+0.006$ |
| 61.0 | $1.780 \pm 0.000$ | $135.39 \pm 0.00$ |  |  |  | 61.0 | $1.784 \pm 0.001$ | $135.49 \pm 0.00$ |  |  |  | $1.660 \pm 0.006$ |

Table 3.-Comparison of the Observed Temperatures ( ${ }^{\circ} \mathrm{C}$.) for the Jumps of $\mathrm{E} / \mathrm{R} \div \mathrm{I}$ ooo, and the Magnitude of the Jumps for Various Aqueous Ethanol Solutions from o\% to $5 \%$ Ethanol.

| Concentration of ethanol in water |  |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 0\% Ethanol. | $\left\{\begin{array}{l}\text { 1. Temperature of jumps } \\ \text { in (E/R)/1000 }\end{array}\right.$ | 12.4 | 15.5 | 17.5 | 22.0 | 27.4 | 33.8 | 37.1 | 41.6 |  | 49.0 | 55.0 |
| ((i.e. purewater) | 2. Depth of jump. | 0.04 | 0.07 | 0.06 | 0.09 | 0.07 | 0.06 | 0.06 | 0.06 |  | 0.08 | 0.05 |
| $0.9 \%$ ethanol | $\left\{\begin{array}{l}\text { 1. Temperature of jumps } \\ \text { in }(\mathrm{E} / \mathrm{R}) / 1000 \\ \text { 2. Depth of jump. }\end{array}\right.$ | 14.2 0.09 |  | 17.8 0.12 | 23.8 0.10 |  | 30.6 0.09 | 35.8 0.10 | 39.5 0.03 | $\begin{gathered} 44.1 \\ 0.05 \end{gathered}$ | $\begin{gathered} 50.2 \\ 0.12 \end{gathered}$ | $\begin{gathered} 58.8 \\ 0.13 \end{gathered}$ |
| 1.8\% ethanol | $\left\{\begin{array}{l}\text { 1. Temperature of jumps } \\ \text { in }(\mathrm{E} / \mathrm{R}) / 1000 \\ \text { 2. Depth of jump }\end{array}\right.$ | 12.0 0.06 | 15.2 0.07 | 17.6 0.05 | 22.2 0.11 | 25.0 0.03 | 29.0 0.07 | $\begin{gathered} 32.6 \\ 0.13 \end{gathered}$ | $\begin{gathered} 38.6 \\ 0.05 \end{gathered}$ |  |  |  |
| 2.5\% ethanol | $\left\{\begin{array}{l}\text { 1. Temperature of jumps } \\ \text { in }(\mathrm{E} / \mathrm{R}) / 1000 \\ \text { 2. Depth of jump }\end{array}\right.$ | 13.0 0.02 |  | 16.6 0.08 | 20.6 0.12 | $\begin{gathered} 26.0 \\ 0.10 \end{gathered}$ | $\begin{aligned} & 29.1 \\ & 0.05 \end{aligned}$ | $\begin{gathered} 36.2 \\ 0.09 \end{gathered}$ | $\begin{gathered} 40.0 \\ 0.06 \end{gathered}$ | $\begin{gathered} 44.0 \\ 0.04 \end{gathered}$ | $\begin{gathered} 50.2 \\ 0.04 \end{gathered}$ | $\begin{gathered} 55.0 \\ 0.09 \end{gathered}$ |
| 3.5\% ethanol | $\begin{cases}\text { 1. Temperature of jumps } & \\ \text { in }(\mathrm{E} / \mathrm{R}) / 1000 & 10.0 \\ \text { 2. Depth of jump. } & 0.07\end{cases}$ | 12.2 0.12 |  | 16.6 0.11 | 23.0 0.11 | 25.0 0.02 | 29.0 0.10 | 34.0 0.09 | 39.0 0.07 | 45.0 0.05 | 48.0 0.10 | $\begin{gathered} 54.0 \\ 0.09 \end{gathered}$ |
| 4.1\% ethanol | $\begin{cases}\text { 1. Temperature of jumps } & \\ \text { in }(\mathrm{E} / \mathrm{R}) / 1000 & 11.0 \\ \text { 2. Depth of jump. } & 0.11\end{cases}$ | 14.4 0.04 |  | 17.0 0.10 | 19.222 .2 0.090 .03 | 26.0 0.08 | $\begin{gathered} 29.9 \\ 0.07 \end{gathered}$ | $\begin{gathered} 33.5 \\ 0.13 \end{gathered}$ | $\begin{gathered} 40.0 \\ 0.03 \end{gathered}$ | $\begin{gathered} 43.9 \\ 0.04 \end{gathered}$ | 46.5 0.04 | $\begin{gathered} 51.0 \\ 0.06 \end{gathered}$ |
| 5\% ethanol | $\left\{\begin{array}{l}\text { 1. Temperature of jumps } \\ \text { in }(\mathrm{E} / \mathrm{R}) / 1000 \\ \text { 2. Depth of jump. }\end{array}\right.$ | 13.6 0.10 |  | 17.0 0.08 | $\begin{gathered} 20.923 .9 \\ 0.110 .08 \end{gathered}$ | 26.9 0.02 | 28.8 0.04 | 33.9 0.08 | $\begin{gathered} 38.3 \\ 0.09 \end{gathered}$ | $\begin{gathered} 43.8 \\ 0.09 \end{gathered}$ | $\begin{gathered} 50.4 \\ 0.03 \end{gathered}$ |  |

In order to decide the precise position and nature of these branchings, further investigations on the intermediate concentrations are necessary so as to trace out fully the course of each of these discontinuities, as was done in the case of some concentrated ethanol solutions. 8 The experiments on some more concentrations are in hand and will be reported later.

Acknowledgement.-The authors are highly indebted to their supervisor, Dr. M.M. Qurashi Chief Scientist, Defence Science Organization, Ministry of Defence, Government of Pakistan, Rawalpindi, for his kind guidance during the course of these investigations.

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